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the facility meets the requirements of either §98.2(a)(1) or (2).

§ 98.82 GHGs to report.

You must report:

- (a) CO_2 process emissions from calcination in each kiln.
- (b) CO_2 combustion emissions from each kiln.
- (c) CH_4 and N_2O combustion emissions from each kiln. You must calculate and report these emissions under subpart C of this part (General Stationary Fuel Combustion Sources) by following the requirements of subpart C.
- (d) CO_2 , CH_4 , and N_2O emissions from each stationary combustion unit other than kilns. You must report these emissions under subpart C of this part (General Stationary Fuel Combustion Sources) by following the requirements of subpart C.

§ 98.83 Calculating GHG emissions.

You must calculate and report the annual process CO_2 emissions from each kiln using the procedure in paragraphs (a) and (b) of this section.

(a) For each cement kiln that meets the conditions specified in §98.33(b)(4)(ii) or (b)(4)(iii), you must calculate and report under this subpart the combined process and combustion

 CO_2 emissions by operating and maintaining a CEMS to measure CO_2 emissions according to the Tier 4 Calculation Methodology specified in §98.33(a)(4) and all associated requirements for Tier 4 in subpart C of this part (General Stationary Fuel Combustion Sources).

- (b) For each kiln that is not subject to the requirements in paragraph (a) of this section, calculate and report the process and combustion CO₂ emissions from the kiln by using the procedure in either paragraph (c) or (d) of this section.
- (c) Calculate and report under this subpart the combined process and combustion CO_2 emissions by operating and maintaining a CEMS to measure CO_2 emissions according to the Tier 4 Calculation Methodology specified in \$98.33(a)(4)\$ and all associated requirements for Tier 4 in subpart C of this part (General Stationary Fuel Combustion Sources).
- (d) Calculate and report process and combustion CO_2 emissions separately using the procedures specified in paragraphs (d)(1) through (d)(4) of this section.
- (1) Calculate CO_2 process emissions from all kilns at the facility using Equation H–1 of this section:

$$CO_{2CMF} = \sum_{m=1}^{k} CO_{2Cli,m} + CO_{2rm}$$
 (Eq. H-1)

Where:

 ${
m CO_2}$ $_{
m CMF}$ = Annual process emissions of ${
m CO_2}$ from cement manufacturing, metric tons.

 ${
m CO_2}_{{
m Cli},m}$ = Total annual emissions of ${
m CO_2}_{
m from}$ clinker production from kiln m, metric tons.

 $\rm CO_{2~rm}$ = Total annual emissions of $\rm CO_{2}$ from raw materials, metric tons.

k = Total number of kilns at a cement manufacturing facility.

(2) CO_2 emissions from clinker production. Calculate CO_2 emissions from each kiln using Equations H–2 through H–5 of this section.

$$CO_{2\ Cli,m} = \sum_{j=1}^{p} \left[\left(Cli_{,j} \right) * \left(EF_{Cli,j} \right) * \frac{2000}{2205} \right] + \sum_{j=1}^{r} \left[\left(CKD_{,i} \right) * \left(EF_{CKD,j} \right) * \frac{2000}{2205} \right]$$
 (Eq. H-2)

Where:

Cli, = Quantity of clinker produced in month j from kiln m, tons.

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 ${\rm EF_{Cli,j}}={\rm Kiln}$ specific clinker emission factor for month j for kiln m, metric tons ${\rm CO_2/}$ metric ton clinker computed as specified in Equation H–3 of this section.

CKD, i = Cement kiln dust (CKD) not recycled to the kiln in quarter i from kiln m, tons. EF_{CKD,i} = Kiln specific CKD emission factor for quarter i from kiln m, metric tons CO₂/metric ton CKD computed as specified in

Equation H-4 of this section.

p = Number of months for clinker calculation, 12.

r = Number of quarters for CKD calculation,

2000/2205 =Conversion factor to convert tons to metric tons.

(i) Kiln-Specific Clinker Emission Factor. (A) Calculate the kiln-specific clinker emission factor using Equation H-3 of this section.

$$EF_{\text{Cli}} = \left(CLi_{CaO} - Cli_{ncCaO}\right) * MR_{CaO} + \left(Cli_{MgO} - Cli_{ncMgO}\right) * MR_{MgO}$$
 (Eq. H-3)

Where:

 ${
m Cli_{CaO}}={
m Monthly}$ total CaO content of Clinker, wt-fraction.

 ${
m Cli}_{
m ncCaO} = {
m Monthly\ non-calcined\ CaO}$ content of Clinker, wt-fraction.

 $\rm MR_{\rm CaO} = Molecular\mbox{-weight}$ Ratio of $\rm CO_2/CaO = 0.785.$

 $\operatorname{Cli}_{\operatorname{MgO}} = \operatorname{Monthly}$ total MgO content of Clinker, wt-fraction.

 ${
m Cli_{ncMgO}}={
m Monthly}$ non-calcined MgO content of Clinker, wt-fraction.

 MR_{MgO} = Molecular-weight Ratio of CO_2/MgO = 1.092.

(B) Non-calcined CaO is CaO that remains in the clinker in the form of

 ${\rm CaCO_3}$ and ${\rm CaO}$ in the clinker that entered the kiln as a non-carbonate species. Non-calcined MgO is MgO that remains in the clinker in the form of MgCO₃ and MgO in the clinker that entered the kiln as a non-carbonate species

(ii) Kiln-Specific CKD Emission Factor.
(A) Calculate the kiln-specific CKD emission factor for CKD not recycled to the kiln using Equation H-4 of this section.

$$EF_{\text{CKD}} = \left(CKD_{CaO} - CKD_{ncCaO}\right) * MR_{CaO} + \left(CKD_{MgO} - CKD_{ncMgO}\right) * MR_{MgO}$$
 (Eq. H-4)

Where:

 $\begin{array}{lll} CKD_{CaO} &=& Quarterly \ total \ CaO \ content \ of \\ CKD \ not \ recycled \ to \ the \ kiln, \ wt-fraction. \\ CKD_{CaO} &=& Quarterly \ non-calcined \ CaO \ content \ of \ CKD \ not \ recycled \ to \ the \ kiln, \ wt-fraction. \\ \end{array}$

 $\mathrm{MR}_{\mathrm{CaO}}=\mathrm{Molecular}\text{-weight Ratio of CO}_2/\mathrm{CaO}=0.785.$

 $\begin{array}{lll} CKD_{MgO} = & Quarterly \ total \ MgO \ content \ of \\ CKD \ not \ recycled \ to \ the \ kiln, \ wt-fraction. \\ CKD_{MgO} = & Quarterly \ non-calcined \ MgO \ content \ of \ CKD \ not \ recycled \ to \ the \ kiln, \ wt-fraction. \\ \end{array}$

 MR_{MgO} = Molecular-weight Ratio of CO_2/MgO = 1.092.

(B) Non-calcined CaO is CaO that remains in the CKD in the form of $CaCO_3$ and CaO in the CKD that entered the kiln as a non-carbonate species. Non-calcined MgO is MgO that remains in the CKD in the form of $MgCO_3$ and MgO in the CKD that entered the kiln as a non-carbonate species.

(3) CO_2 emissions from raw materials. Calculate CO_2 emissions from raw materials using Equation H–5 of this section:

$$CO_{2,rm} = \sum_{i=1}^{m} rm * TOCrm * \frac{44}{12} * \frac{2000}{2205}$$
 (Eq. H-5)

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Where:

rm = The amount of raw material i consumed annually, tons/yr (dry basis) or the amount of raw kiln feed consumed annually, tons/yr (dry basis).

 $CO_{2,rm}$ = Annual CO_2 emissions from raw materials.

TOCrm = Organic carbon content of raw material i or organic carbon content of combined raw kiln feed (dry basis), as determined in §98.84(c) or using a default factor of 0.2 percent of total raw material weight.

M = Number of raw materials or 1 if calculating emissions based on combined raw kiln feed.

44/12 = Ratio of molecular weights, CO_2 to carbon.

2000/2205 = Conversion factor to convert tons to metric tons.

(4) Calculate and report under subpart C of this part (General Stationary Fuel Combustion Sources) the combustion CO_2 emissions from the kiln according to the applicable requirements in subpart C.

[74 FR 56374, Oct. 30, 2009, as amended at 75 FR 66461, Oct. 28, 2010]

§98.84 Monitoring and QA/QC requirements.

(a) You must determine the weight fraction of total CaO and total MgO in CKD not recycled to the kiln from each kiln using ASTM C114-09, Standard Test Methods for Chemical Analysis of Hydraulic Cement (incoporated by reference, see §98.7). The monitoring must be conducted quarterly for each kiln from a CKD sample drawn either as CKD is exiting the kiln or from bulk CKD storage.

(b) You must determine the weight fraction of total CaO and total MgO in clinker from each kiln using ASTM C114-09 Standard Test Methods for Chemical Analysis of Hydraulic Cement (incorporated by reference, see §98.7). The monitoring must be conducted monthly for each kiln from a monthly clinker sample drawn from bulk clinker storage if storage is dedicated to the specific kiln, or from a monthly arithmetic average of daily clinker samples drawn from the clinker conveying systems exiting each kiln.

(c) The total organic carbon content (dry basis) of raw materials must be determined annually using ASTM C114-09 Standard Test Methods for Chemical Analysis of Hydraulic Cement (incorporated by reference, see §98.7) or a similar industry standard practice or method approved for total organic carbon determination in raw mineral materials. The analysis must be conducted either on sample material drawn from bulk raw kiln feed storage or on sample material drawn from bulk raw material storage for each category of raw material (i.e., limestone, sand, shale, iron oxide, and alumina). Facilities that opt to use the default total organic carbon factor provided in §98.83(d)(3), are not required to monitor for TOC.

(d) The quantity of clinker produced monthly by each kiln must be determined by direct weight measurement of clinker using the same plant techniques used for accounting purposes, such as reconciling weigh hopper or weigh feeder measurements against inventory measurements. As an alternative, facilities may also determine clinker production by direct measurement of raw kiln feed and application of a kiln-specific feed-toclinker factor. Facilities that opt to use a feed-to-clinker factor must verify the accuracy of this factor on a monthly basis.

(e) The quantity of CKD not recycled to the kiln generated by each kiln must be determined quarterly using the same plant techniques used for accounting purposes, such as direct weight measurement using weigh hoppers, truck weigh scales, or belt weigh feeders.

(f) The annual quantity of raw kiln feed or annual quantity of each category of raw materials consumed by the facility (e.g., limestone, sand, shale, iron oxide, and alumina) must be determined monthly by direct weight measurement using the same plant instruments used for accounting purposes, such as weigh hoppers, truck weigh scales, or belt weigh feeders.

(g) The monthly non-calcined CaO and MgO that remains in the clinker in the form of CaCO₃ or that enters the kiln as a non-carbonate species may be assumed to be a default value of 0.0 or may be determined monthly by careful chemical analysis of feed material and clinker material from each kiln using well documented analytical and

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